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HYDRAULIC MODEL STUDIES OF CORRUGATED-METAL PIPE UNDERDRAIN ENERGY DISSIPATORS

D. Colgate
Engineering and Research Center
Bureau of Reclamation

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Prepared for
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by
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Prepared for
FOREST SERVICE

Hydraulics Branch
Division of General Research
Engineering and Research Center
Denver, Colorado

UNITED STATES DEPARTMENT OF THE INTERIOR
Rogers C. B. Morton
Secretary

*

BUREAU OF RECLAMATION
Ellis L. Armstrong
Commissioner

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Table II

QUANTITIES AND UNITS OF MECHANICS

Multiply	By	To obtain
MASS		
Grains (1/7,000 lb)	64.79891 (exactly)	Milligrams
Troy ounces (480 grains)	31.1035	Grams
Ounces (avdp)	28.3495	Grams
Pounds (avdp)	0.45359237 (exactly)	Kilograms
Short tons (2,000 lb)	907.185	Kilograms
	0.907185	Metric tons
Long tons (2,240 lb)	1,016.05	Kilograms
FORCE/AREA		
Pounds per square inch	0.070307	Kilograms per square centimeter
	0.689476	Newtons per square centimeter
Pounds per square foot	4.88243	Kilograms per square meter
	47.8803	Newtons per square meter
MASS/VOLUME (DENSITY)		
Ounces per cubic inch	1.72999	Grams per cubic centimeter
Pounds per cubic foot	16.0185	Kilograms per cubic meter
	0.0160185	Grams per cubic centimeter
Tons (long) per cubic yard	1.32894	Grams per cubic centimeter
MASS/CAPACITY		
Ounces per gallon (U.S.)	7.4893	Grams per liter
Ounces per gallon (U.K.)	6.2362	Grams per liter
Pounds per gallon (U.S.)	119.829	Grams per liter
Pounds per gallon (U.K.)	99.779	Grams per liter
BENDING MOMENT OR TORQUE		
Inch-pounds	0.011521	Meter-kilograms
	1.12985×10^6	Centimeter-dynes
Foot-pounds	0.138255	Meter-kilograms
	1.35582×10^7	Centimeter-dynes
Foot-pounds per inch	5.4431	Centimeter-kilograms per centimeter
Ounce-inches	72.008	Gram-centimeters
VELOCITY		
Feet per second	30.48 (exactly)	Centimeters per second
	0.3048 (exactly)*	Meters per second
Feet per year	0.965873×10^{-6}*	Centimeters per second
Miles per hour	1.609344 (exactly)	Kilometers per hour
	0.44704 (exactly)	Meters per second
ACCELERATION*		
Feet per second^2	0.3048*	Meters per second^2
FLOW		
Cubic feet per second (second-feet)	0.028317*	Cubic meters per second
Cubic feet per minute	0.4719	Liters per second
Gallons (U.S.) per minute	0.06309	Liters per second
FORCE*		
Pounds	0.453592*	Kilograms
	4.4482*	Newtons
	4.4482×10^{-5}*	Dynes

Multiply	By	To obtain
WORK AND ENERGY*		
British thermal units (Btu)	0.252*	Kilogram calories
	1,055.06	Joules
Btu per pound	2.326 (exactly)	Joules per gram
Foot-pounds	1.35582*	Joules
POWER		
Horsepower	745.700	Watts
Btu per hour	0.293071	Watts
Foot-pounds per second	1.35582	Watts
HEAT TRANSFER		
Btu in./hr ft^2 deg F (k, thermal conductivity)	1.442	Milliwatts/cm deg C
	0.1240	Kg cal/hr m deg C
Btu ft/hr ft^2 deg F	1.4880*	Kg cal m/hr m^2 deg C
Btu/hr ft^2 deg F (C, thermal conductance)	0.568	Milliwatts/cm^2 deg C
	4.882	Kg cal/hr m^2 deg C
Deg F hr ft^2/Btu (R, thermal resistance)	1.761	Deg C cm^2/milliwatt
Btu/lb deg F (c, heat capacity)	4.1868	J/g deg C
Btu/lb deg F	1.000*	Cal/gram deg C
Ft^2/hr (thermal diffusivity)	0.2581	Cm^2/sec
	0.09290*	M^2/hr
WATER VAPOR TRANSMISSION		
Grains/hr ft^2 (water vapor transmission)	16.7	Grams/24 hr m^2
Perms (permeance)	0.659	Metric perms
Perm-inches (permeability)	1.67	Metric perm-centimeters

Table III

OTHER QUANTITIES AND UNITS

Multiply	By	To obtain
Cubic feet per square foot per day (seepage)	304.8*	Liters per square meter per day
Pound-seconds per square foot (viscosity)	4.8824*	Kilogram second per square meter
Square feet per second (viscosity)	0.092903*	Square meters per second
Fahrenheit degrees (change)*	5/9 exactly	Celsius or Kelvin degrees (change)*
Volts per mil	0.03937	Kilovolts per millimeter
Lumens per square foot (foot-candles)	10.764	Lumens per square meter
Ohm-circular mils per foot	0.001662	Ohm-square millimeters per meter
Millicuries per cubic foot	35.3147*	Millicuries per cubic meter
Milliamps per square foot	10.7639*	Milliamps per square meter
Gallons per square yard	4.527219*	Liters per square meter
Pounds per inch	0.17858*	Kilograms per centimeter

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PURPOSE

These studies were made to develop self-cleaning energy dissipators to be placed at the outlet ends of corrugated-metal-pipe culverts under trails and roadways.

RESULTS

1. The hydraulic model study produced a basic design for energy dissipators to be used with either annular or helical corrugated-metal pipe. The pipe may be any size up to 36 inches.

2. The dissipator operates satisfactorily for pipe slopes between 0 and 66-2/3 percent. A slight modification to the basic design is required for slopes greater than 40 percent.

3. The energy head ($V^2/2g$ plus flow depth) in an 18-inch corrugated-metal pipe may be as great as 10 feet.

4. The energy dissipator is self-cleaning for either rocks or floating debris.

5. The dissipator will operate satisfactorily regardless of backwater elevation.

6. By using the data presented in Figures 7, 10, and 18, an energy dissipator may be dimensioned for any installation.

APPLICATION

The energy dissipator may be used to prevent scour at the outfall of small underdrains for trails or roadways.

INTRODUCTION

The Forest Service, U.S. Department of Agriculture, requested the Bureau of Reclamation to design an energy dissipator to be used at the outfall end of small underdrains. An energy dissipator was needed to prevent the scour and undercutting which occurred during each operating season and which required extensive yearly maintenance to these structures (Figure 1).

The following requirements were set forth by the Forest Service and were used as guidelines during the laboratory development of the dissipator:

Figure 1. Unprotected field underdrain. Scour at outfall end of 12-inch underdrain. Photo PX-D-68551

1. The basic energy dissipator would accommodate an 18-inch corrugated-metal pipe, either annular or helical. Pipe slopes would vary from 0 to 66-2/3 percent, and the maximum energy head in the pipe would be 10 feet.

2. The design would stress simplicity so that parts of a unit energy dissipator could be handled manually and be readily assembled in place. The dissipator could not be rigidly attached to, nor support, the pipe.

3. The energy dissipator would be self-cleaning of soil, rocks (up to 6 inches), and floating debris, but would be so designed that manual cleaning could be easily performed.

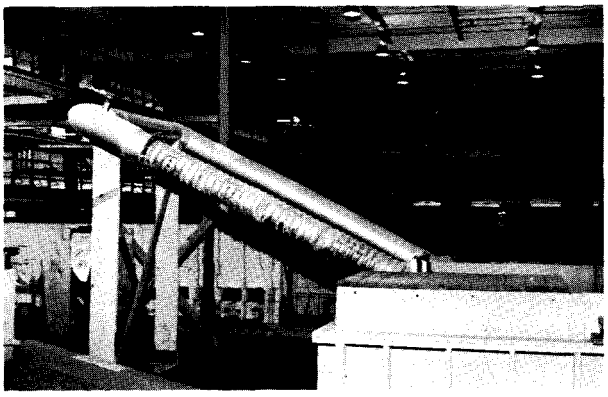
4. Any dissipator part subjected to wear from impact by objects carried in the flowing water should be easily replaced as maintenance required.

5. Dissipators should be developed for each of three energy head ranges: 0 to 2.5 feet, 2.5 to 5.0 feet, and 5.0 to 10.0 feet. Exit velocities for the energy head range 0 to 5 feet should be 2 fps, and the 5- to 10-foot range should be 3.5 fps. (Note: This requirement was deleted by the Forest Service representative as discussed later.)

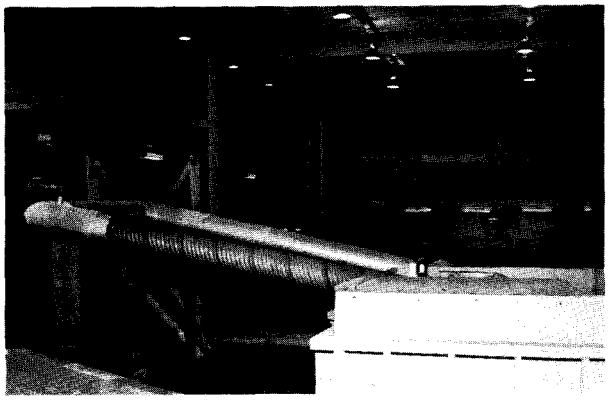
THE MODEL

Two 10-foot sections of 10-inch corrugated-metal pipe, one annular and one helical, were obtained commercially to represent pipe underdrains. The model

scale, 1:1.8, was thus set, and all basic studies were based on the hydraulic characteristics of an 18-inch corrugated-metal pipe. Trunnions were mounted on the horizontal centerline of the pipe 9 inches from the outfall end, and the laboratory piping was so arranged that a dresser coupling could be installed in line with the axis of the trunnions. By rotating the pipe test section and its lead-in piping around the trunnion–dresser coupling axis, any desired corrugated-metal pipe slope from 0 to 66-2/3 percent could be set (Figure 2).



A. 10-inch annular corrugated-metal pipe S = 66-2/3 percent. Photo PX-D-68541



B. 10-inch helical corrugated-metal pipe S = 10 percent. Photo PX-D-68547

Figure 2. Laboratory installation.

Water for the study was furnished to the system by the permanently installed laboratory pumps, and passed through any selected one of five venturi meters. The laboratory system could deliver and accurately measure any model flow representing up to 46.5 cfs, which is the discharge through an 18-inch corrugated-metal pipe flowing full on a 66-2/3 percent slope.

The corrugated-metal pipe outfall terminated in a watertight box 10 feet square in plan, and 5 feet deep. Water depth in the box could be adjusted up to the elevation of the pipe outfall centerline (Figure 3). The various energy dissipator configurations desired for study could be readily installed in the watertight box and adjusted in location with respect to the pipe outfall. Thus, pipe slope, discharge, and tailwater depth could be adjusted for each energy dissipator configuration.

THE INVESTIGATION

Floor and Sidewall Study

Adjustable floor and sidewall panels were installed in the model box with the exit end of the floor 72 inches wide, 43 inches below, and 75 inches downstream from the corrugated-metal-pipe trunnions (Figure 4). The sidewalls were vertical. The tailwater was varied to study flow patterns as floor and sidewalls were rotated about the downstream end of the dissipator (Figure 5). The jet from the pipe concentrated in the center of the energy dissipator at all discharges, and skipped across the water surface at high tailwater. The deep pool at the downstream end of the dissipator appeared to be unnecessary.

Partial floor panels, which were so designed that the exit end could be sloped upward into the stream, were installed at various locations downstream from the pipe outfall, and a baffle panel was placed in the path of the jet to spread it and deflect the flow downward (Figure 4A). For all configurations tested, the flow swept out of the dissipator for energy heads greater than about 2.2 feet (Figure 6).

Baffle and Deflector Study

The previous study indicated that the baffle panel was very effective in spreading and directing the jet downward. A study was made with various baffle panels and a deep upstream pool (Figure 4C). Flow was deflected downward parallel to the face of the baffle,

and could be directed back upstream by adding a deflector to the bottom edge of the baffle. With the proper combination of baffle, deflector, and an upward sloping floor extending downstream from the plane of the baffle, the hydraulic jump could be held upstream from the baffle for all discharges and backwater elevations.

Exit Width Computation

A mathematical study was made concerning the requirement of a free discharge velocity of 2 fps for energy heads up to 5 feet, and 3.5 fps for energy heads between 5 and 10 feet. The flow will pass through critical velocity (Vc) as it leaves the exit end of the energy dissipator in a free discharge mode. The required width (W) of the energy dissipator exit for any assigned critical velocity and discharge (Q) may be computed from the relationship

$$W = \frac{Qg}{Vc^3}$$

where g is the acceleration of gravity. With the suggested maximum free flow exit velocity of 2 fps, and the maximum discharge of 25.5 cfs for an energy head of 5 feet, the required energy dissipator exit width would be over 100 feet. In view of the impractical widths necessary to meet the suggested maximum exit velocities, representatives of the Forest Service deleted the exit velocity requirements.

RECOMMENDED DESIGN

Basic Energy Dissipator

The optimum configuration for each part of the energy dissipator were combined to form a basic energy dissipator. The 1:1.8 scale model dimensions are shown in Figure 4D.

The recommended basic energy dissipator configuration for an 18-inch corrugated-metal pipe is shown in Figure 7. The baffle and deflector location, upstream dissipator width, downstream wall divergence, and exit lip elevation must be considered as critical dimensions. Other dimensions shown such as splash guard locations, slight slope to the upstream floor, and wall height, may be varied for given locations and discharge requirements. The recommended design, fabricated of sheet metal, is shown installed in the watertight tail box in Figure 8, and in detail in Figure 9.

Positioning the Corrugated-metal Pipe Outfall

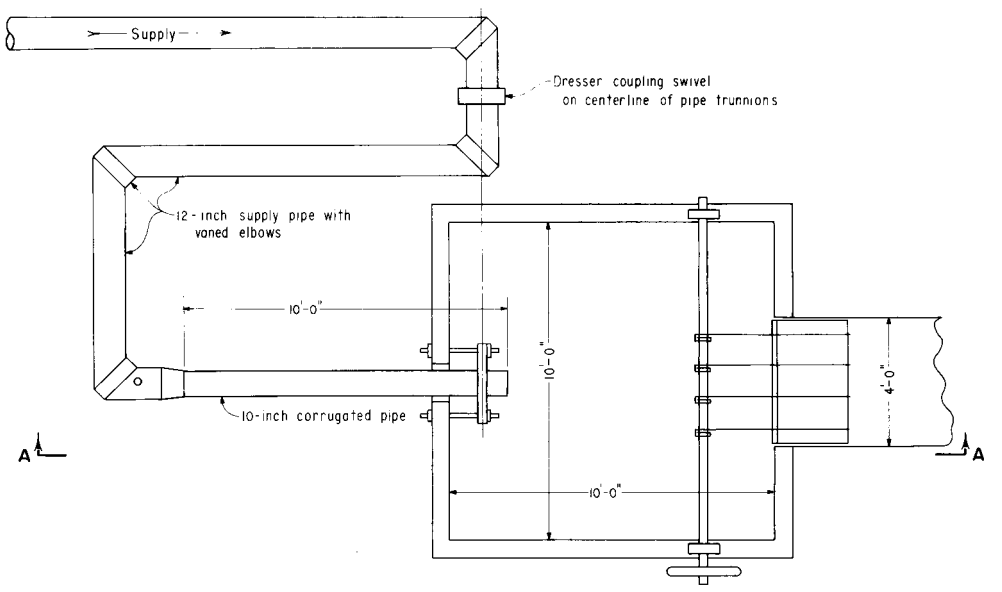
For proper energy dissipation and self-cleaning of the energy dissipator, the lower surface of the jet from the corrugated-metal pipe must strike the baffle at or near the intersection of the baffle and the deflector. The optimum location of the bottom of the pipe in relation to the baffle and deflector for the basic energy dissipator is shown in Figure 10. The minimum horizontal distance shown, one pipe diameter or 18 inches, is arbitrary with respect to energy dissipation, but is considered a safe minimum distance to permit clearance of debris discharging from the pipe.

The pipe outfall positioning as shown in Figure 10 will permit satisfactory energy dissipation for all pipe slopes as shown. However, for the steeper slopes and higher vertical positions (above 40 inches), some splash over the walls of the dissipator and the top of the baffle splash guard should be expected. Some additional splash protection may be required for these extreme conditions depending on the dissipator location and discharge requirements.

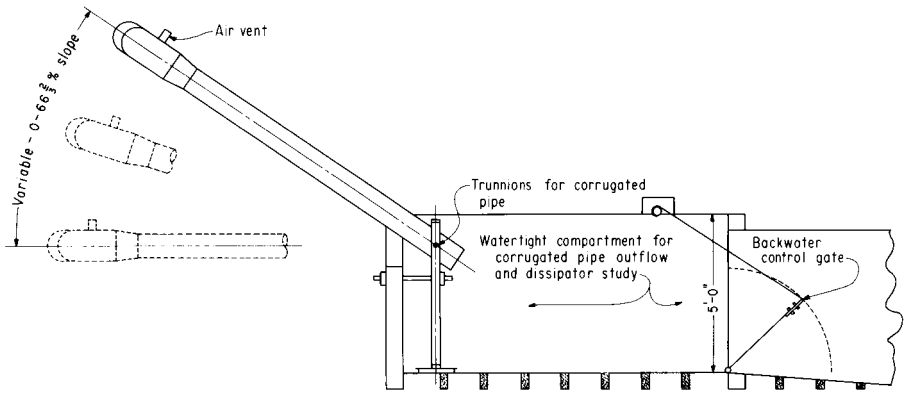
Splash Guards

A strong component of the jet from the pipe will be deflected upward along the vertical face of the baffle. This high-velocity sheet of water, when deflected upstream by the "lip" on top of the baffle plate, will cause excessive splash (Figure 11A). A splash guard attached to the upstream edge of the lip extension will return the sheet of water downward and eliminate the unsatisfactory splash and spray as shown in Figure 11B. The recommended baffle splash guard dimensions are shown in Figure 7.

In this model study, an annular ring of open area existed between the corrugated pipe and the backplate of the energy dissipator since the pipe was not rigidly attached to the dissipator. The backplate was subjected to random jets and surging, and a large flow of water issued out between the pipe and the backplate (Figure 11A). This flow would tend to scour the bedding material around the outfall end of the corrugated-metal pipe and around the dissipator. A 4-inch-wide splash guard or deflector as shown in Figure 7 is recommended for installation on the backplate to protect the intersection of the pipe and backplate from direct jets or surges.



PLAN



ELEVATION A-A

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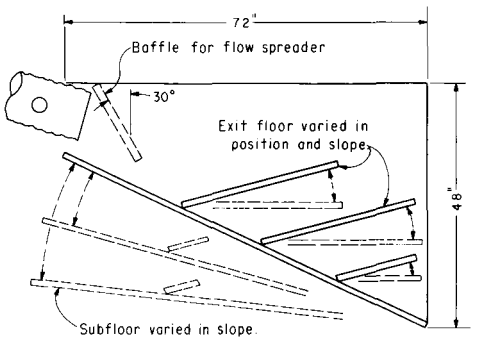
DIVISION OF GENERAL RESEARCH
DENVER, COLORADO

757

FOREST SERVICE
ENERGY DISSIPATOR
FOR
18-INCH CORRUGATED PIPE

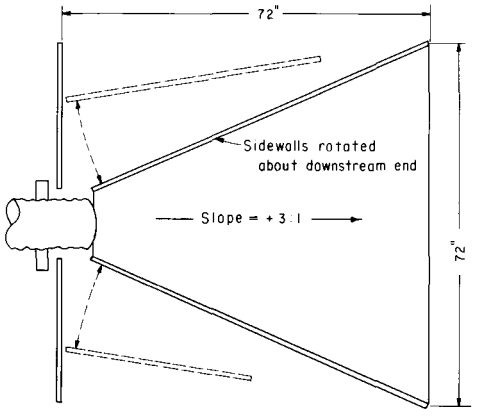
Figure 3. Model drawing, laboratory installation for 1:1.8 scale model study.



ELEVATION

A. FLOOR STUDY

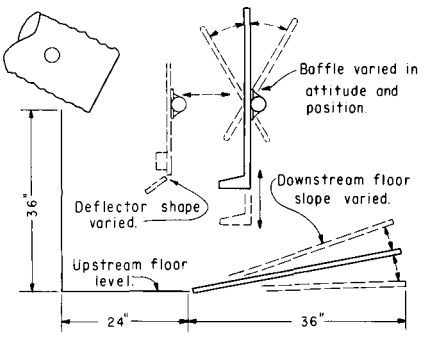
Floor slopes were varied from +4.0:1 to -2.5:1, with reverse slopes at various stations.
The flow from the corrugated pipe did not form a jump, but continued at super-critical velocity across the end sill (See figure 6)



PLAN

B. SIDE WALL STUDY

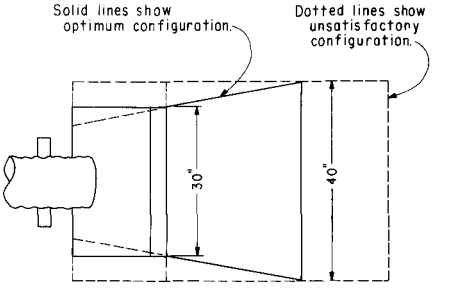
Side walls were vertical and symetrical about the centerline.
Best flow was obtained with the sidewalls diverging about 20°



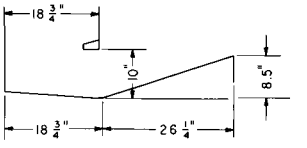
ELEVATION

C. BAFFLE AND DEFLECTOR STUDY

A baffle was designed to direct the jet from the corrugated pipe downward. A deflector was added to return the jet toward the back wall.
Best action was achieved with a vertical baffel and a slightly sloping deflector. Best elevation for the deflector was one pipe diameter above the horizontal floor. The baffle position varied with the pipe slope.



PLAN



ELEVATION

D. COMBINED DISSIPATOR SHAPE STUDY

Optimum energy dissipator dimensions were determined by combining the results of studies A through C.
Self-cleaning potential using both rock and floating debris was determined during this study.

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Figure 4. 1:1.8 scale model dissipator variations. Studies to determine the optimum dimensions for the energy dissipator. All dimensions shown are for the 10-inch laboratory model.

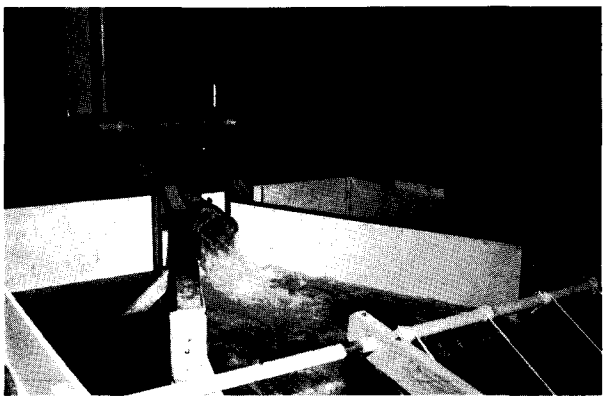

Figure 5. Floor and sidewall study. Photo PX-D-68527

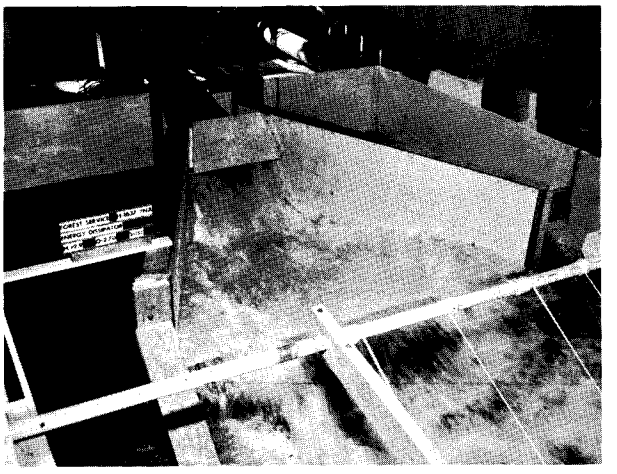

Figure 6. Flow deflector and upward sloping floor. Note sweepout. Photo PX-D-68528

Self-cleaning Capabilities

With the deflector at the bottom of the baffle properly placed, as shown in Figure 7, the jet from the corrugated-metal pipe will be deflected downward along the vertical base of the baffle, and deflected upstream by the deflector to spread laterally and strike the backplate above the floor. A portion of the jet will then be deflected downward to the floor and turned downstream. Thus, the flow on the entire floor of the dissipator will be in the downstream direction and carry with it any loose material on the floor. Random-sized stones were dumped into the pool upstream from the baffle to study the self-cleaning potential of various dissipator designs (Figure 12A). All of the stones were ejected from the energy dissipator within 1 minute (Figure 12B). The design is excellent for self-cleaning of nonfloating debris.

Random lumber scraps were dumped into the pool upstream from the baffle to represent floating debris. These floating particles, in order to be ejected from the energy dissipator, would have to be trapped by the jet from the corrugated-metal pipe, swept under the water surface, and out under the baffle. Many pieces would be repeatedly swept under water only to resurface upstream from the baffle before finally being ejected under the baffle. Twenty-five pieces of scrap lumber dumped into the upstream pool were ejected from the dissipator in about 45 minutes with the dissipator discharging 10 cfs. The ejection of floating debris, although slow, is satisfactory.

For very low flows, below about 15 percent of maximum, the self-cleaning potential of the dissipator is poor.

Slopes Greater than 40 Percent

For pipe slopes greater than 40 percent, the flow from the basic energy dissipator tended to separate from the diverging sidewalls. Large boils appeared near the centerline of the dissipator downstream from the baffle, and eddys or vorticies appeared in the corners at the intersection of the baffle and the diverging sidewalls. The poor flow conditions were more pronounced for steeper pipe slopes.

The addition of two fillers, one on either side of the upstream basin extending from the baffle deflector to splash guard (Figure 13), produced satisfactory flow for all pipe slopes from 40 to 66-2/3 percent. Figure 14 shows the flow conditions for a pipe slope of 40 percent with and without the upstream fillers installed.

For corrugated-metal-pipe slopes less than 40 percent, the fillers tended to concentrate the flow along the diverging sidewalls. The corner fillers (Figure 7), should be used for pipe slopes greater than 40 percent, and should not be used for pipe slopes less than 40 percent. At 40 percent pipe slope the dissipator will operate equally well with or without the corner fillers.

Dissipator Backwater Studies

The dissipator exit lip was placed at the proper elevation to hold sufficient backwater in the exit portion of the dissipator to prevent sweep out. With no backwater downstream from the dissipator, the flow will pass through critical velocity at the exit lip. Figure

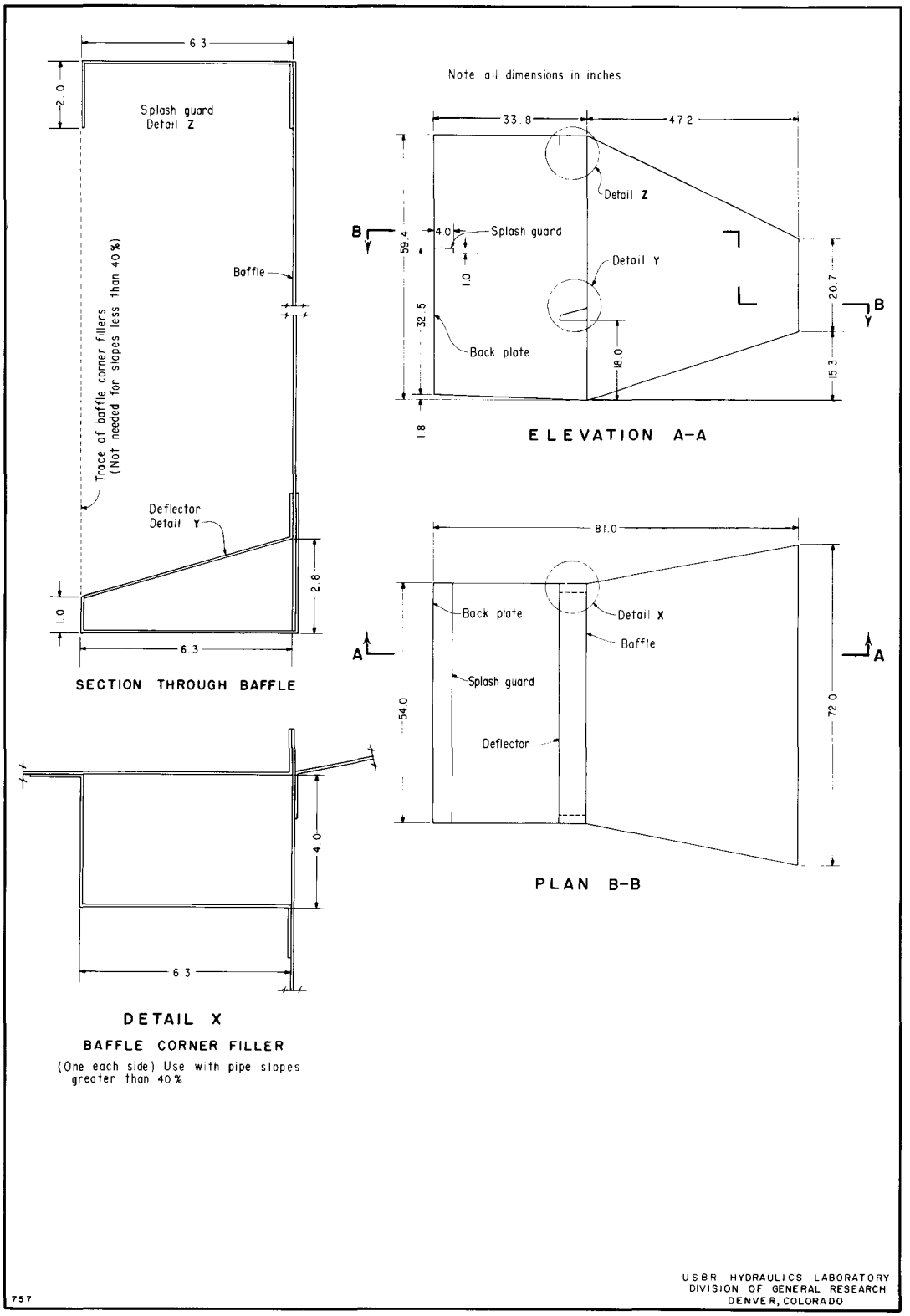

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Figure 7. Basic energy dissipator dimensions

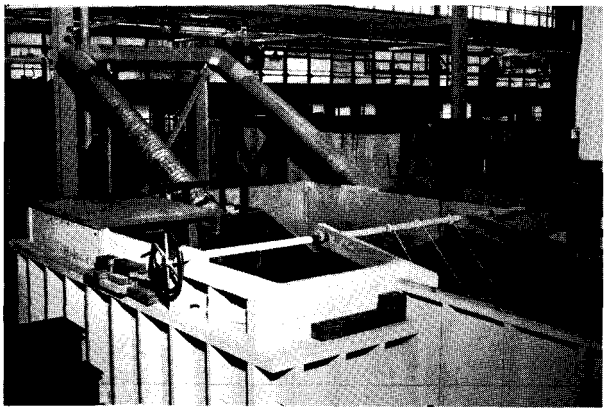


Figure 8. Overall view, typical energy dissipator installation. Pipe slope is 66-2/3 percent. Photo PX-D-68542

15A shows the free outflow conditions with the corrugated-metal pipe entering the upstream basin on a 25 percent slope, an entrance energy head of 5 feet, and a dissipator exit velocity (critical) of 5.2 fps. Some added protection would probably be required in the downstream channel although the exit energy head has been reduced to about 1 foot.

The same entrance flow, 25 percent pipe slope and 5 feet of entrance energy head, was discharged through the system, but with sufficient backwater to produce an average exit velocity of 2.2 fps (Figure 15B). With this low exit velocity little scour would be expected downstream from the energy dissipator.

The dissipator exit conditions for a pipe slope of 25 percent, an entrance energy head of 2.8 feet, and a dissipator exit velocity of about 3.3 fps, is shown in Figure 15C. Although this exit velocity is just critical, the exit flow is tranquil and little scour would be expected.

The backwater study indicated that the energy dissipator will contain the hydraulic jump upstream from the baffle for all discharges, regardless of backwater, but the exit flow from the dissipator will pass through critical velocity at the exit lip unless some type of backwater pool is provided. Where the terrain is such that a backwater pool is not feasible, some channel protection will be needed to protect against scour caused by the critical exit velocity for the maximum design discharge.

Helical Corrugated-metal Pipe

A helical corrugated-metal pipe was installed to discharge into the recommended basic energy

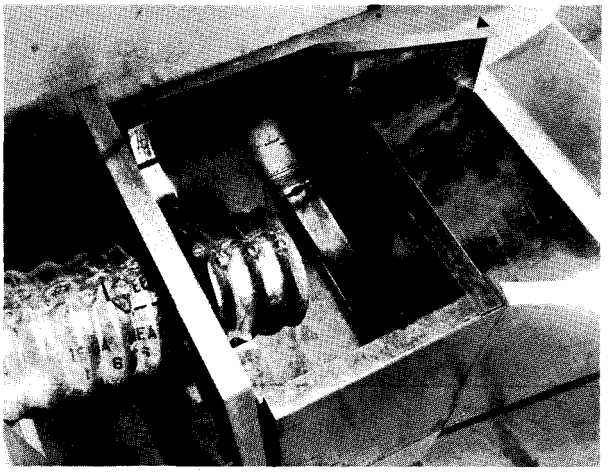
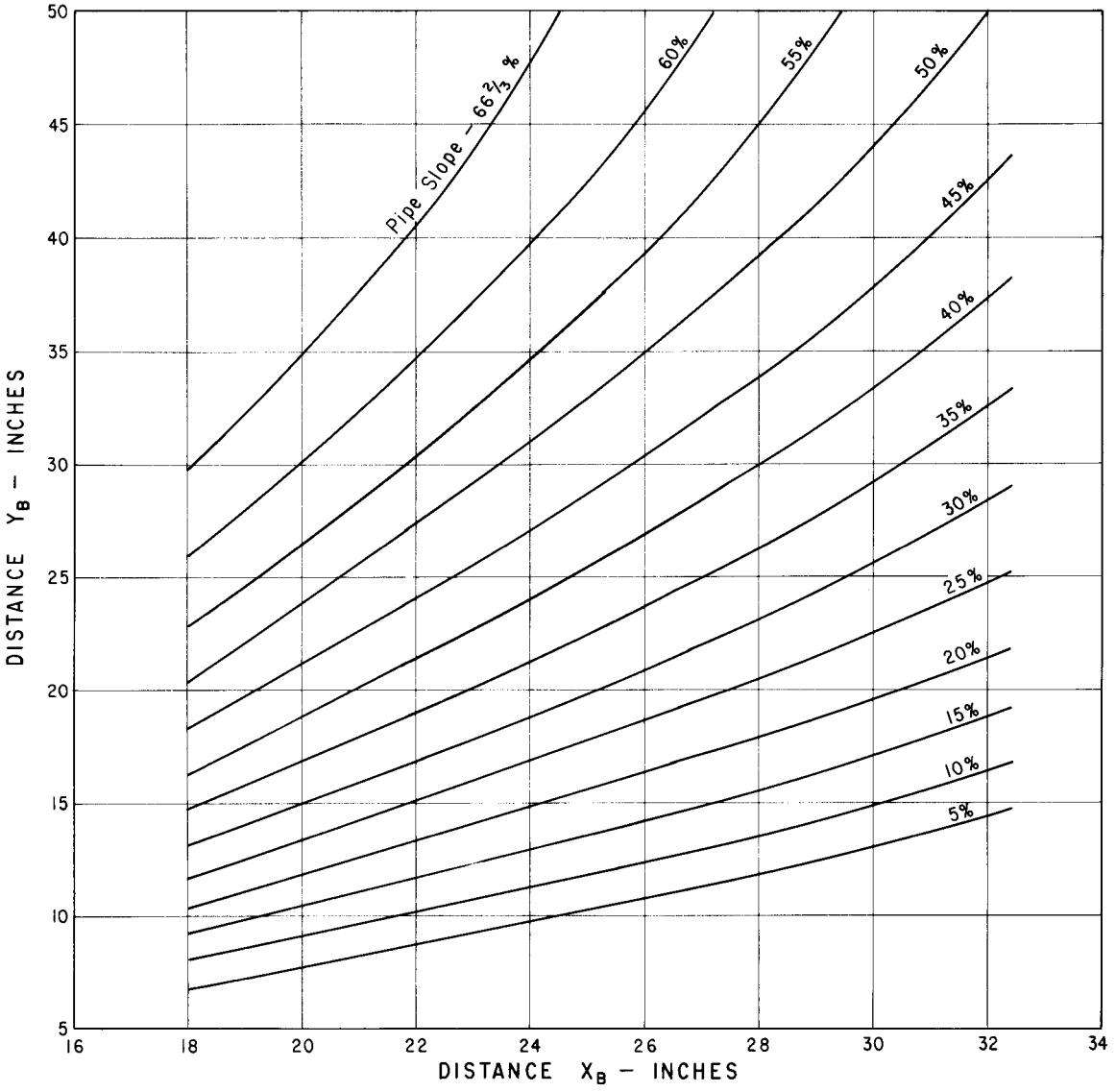


Figure 9. Basic energy dissipator, recommended design. Photo PX-D-68529

dissipator (Figures 2B and 16A). The system was tested with several different pipe slopes, and various X_B–Y_B locations as shown on Figure 10. The performance of the energy dissipator was the same with the helical corrugated-metal pipe as with the annular corrugated-metal pipe. The helical corrugations caused a fin of water to form on the left side at the pipe outfall (Figure 16B); however, except for a slight increase in splash in the upstream basin, the fin did not adversely affect the flow in the energy dissipator. The water in the upstream basin (Figure 16C) and the exit flow from the dissipator was symmetrical for all discharges.

Energy Dissipator Dimension Factors

The recommended basic energy dissipator included the optimum features of all the designs tested for self-cleaning, simplicity, and energy dissipation for an energy head of 5 feet with an 18-inch corrugated-metal pipe flowing full. The basic design produced unsatisfactorily rough flow when the energy head was too great, and unnecessarily tranquil flow when the maximum anticipated energy head was small. A study with the pipe on a slope of 50 percent indicated that the flow from the dissipator was unacceptably rough for an energy head of 8.0 feet (Figure 17A), and undesirably rough for an energy head of 7.2 feet (Figure 17B). These flows produced "boils" and a very rough water surface in the downstream basin which in turn caused uneven flow distribution and relatively high velocity jets to emerge from the dissipator. The flow was acceptable for an energy head of 6.2 feet (Figure 17C), and quite smooth for an energy head of 5.0 feet (Figure 17D). This study indicated that the



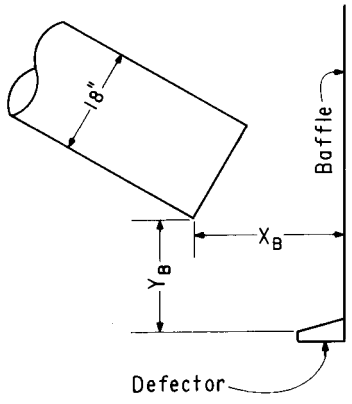


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Figure 10. Location of invert of discharge end of 18-inch corrugated-metal pipe for various pipe slopes.

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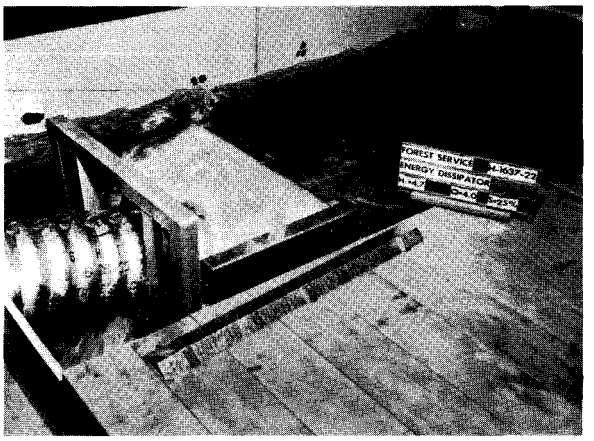
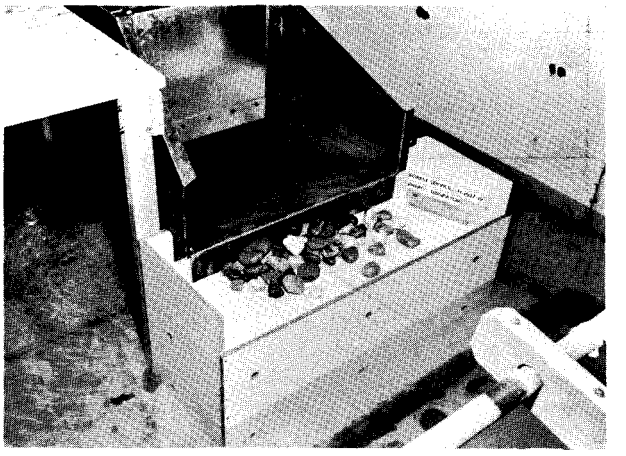


A. No baffle splash guard. Note excessive splash. Photo PX-D-68536

B. With baffle splash guard. Note jet returning to basin. Photo PX-D-68531

Figure 11. Baffle splash guard.

A. Inserting random sized stones upstream from the basin. Photo PX-D-68533



B. All stones were swept from the dissipator within 1 minute. Photo PX-D-68534

Figure 12. Dissipator self-cleaning of stone.

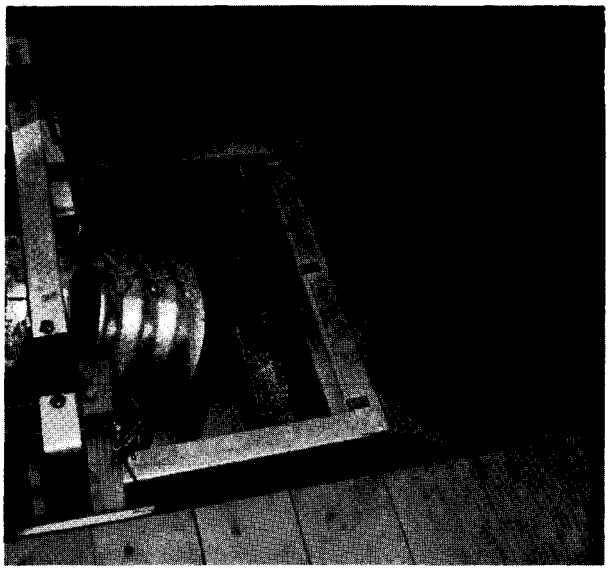


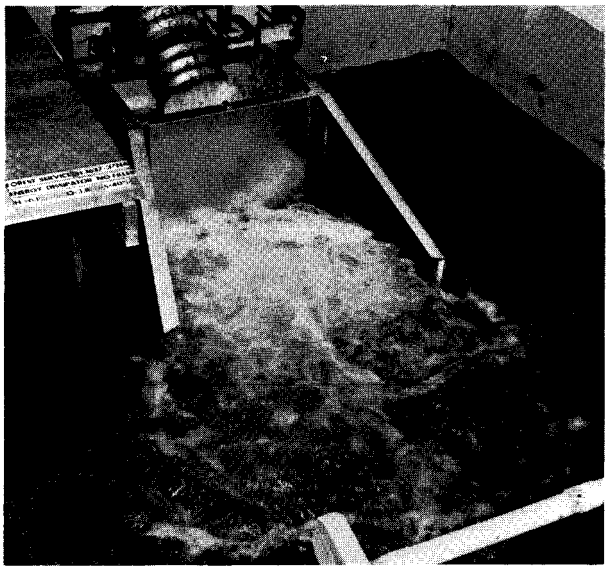
Figure 13. Baffle corner fillers to be used with pipe slopes greater than 40 percent. Photo PX-D-68552

basic design would operate satisfactorily with a pipe slope of 50 percent and a maximum energy head of about 6.7 feet.

A series of studies were made to determine the maximum acceptable energy head for any pipe slope when used with the basic energy dissipator. The values thus determined were plotted on the discharge-energy head curve for each pipe slope, with the resultant line labeled, "basic dissipator" (Figure 18). This basic energy dissipator for an 18-inch pipe has the dimensions shown in Figure 7.

Using the results for the basic energy dissipator as a model, a family of curves was generated to show the minimum size of energy dissipator required to satisfactorily handle the flow through an 18-inch corrugated-metal pipe for any combination of discharge and pipe slope producing energy heads up to 11 feet (Figure 18).

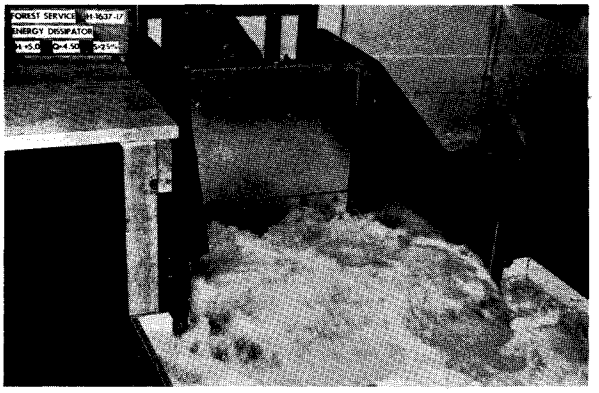
Thus, the dimension factor for an energy dissipator to be used with an 18-inch corrugated-metal pipe for any given pipe slope and maximum discharge may be determined from Figure 18. The dimensions of the dissipator are determined by applying the interpolated dimension factor, or the next higher factor, to all dimensions shown in Figure 7, and to the X_B–Y_B values for the location of the outfall end of the corrugated-metal pipe, Figure 10.



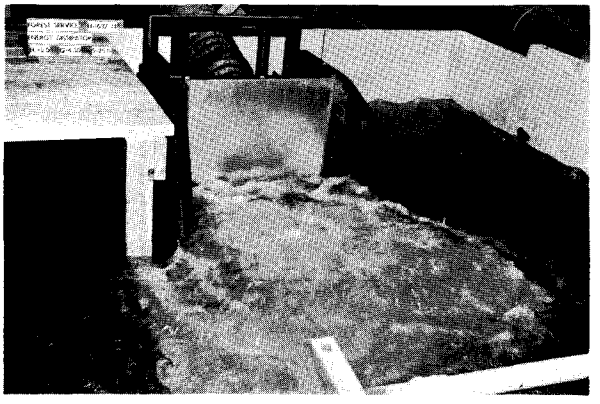
A. Without corner fillers. Photo PX-D-68543

B. With corner fillers. Photo PX-D-68544

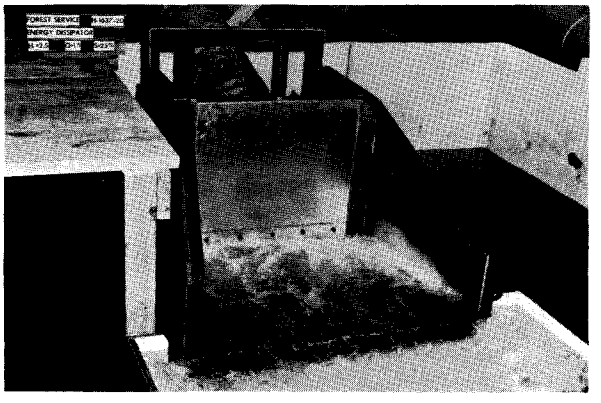
Figure 14. Operation with a pipe slope of 40 percent—with and without baffle corner fillers.



A. Q = 19.5 cfs He = 5.0 feet S = 25 percent Exit depth = 7.6 inches Critical exit V = 5.2 fps (No backwater) Photo PX-D-68532

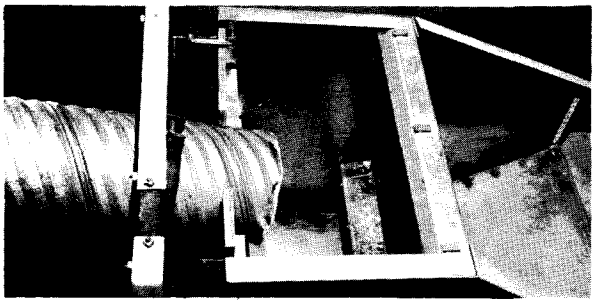


B. Q = 19.5 cfs He = 5.0 feet S = 25 percent Exit depth = 18 inches Exit velocity = 2.2 fps (with backwater) Photo PX-D-68530

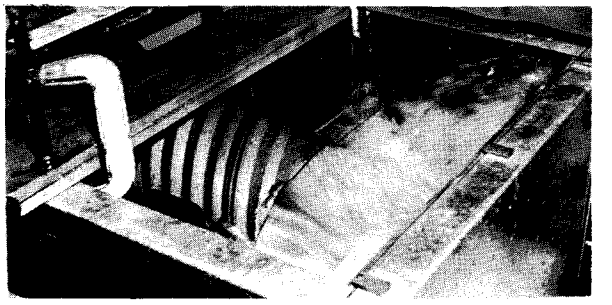


C. Q = 6.5 cfs He = 2.8 feet S = 25 percent Exit depths = 4 inches Critical exit V = 3.3 fps (No backwater) Photo PX-D-68535

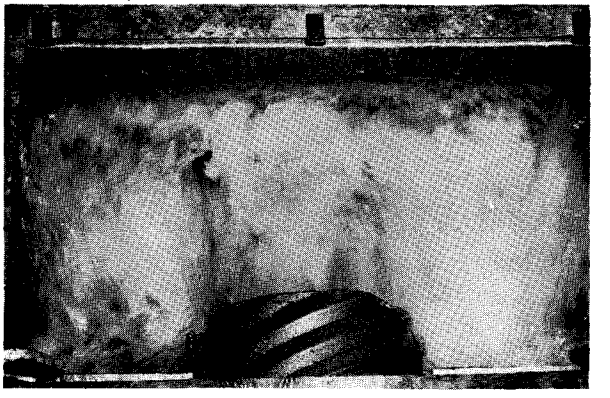
Figure 15. Dissipator exit and backwater conditions.



A. Helical corrugated-metal pipe in the model. Photo PX-D-68548

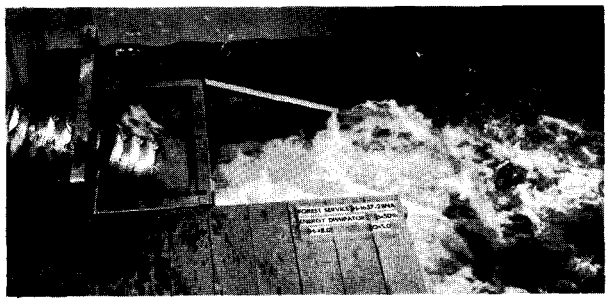


B. Note water fin on left side of exit flow. Photo PX-D-68554

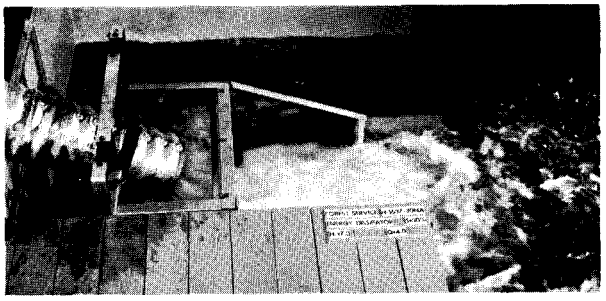


C. Note uniformity in upstream basin. Photo PX-D-68550

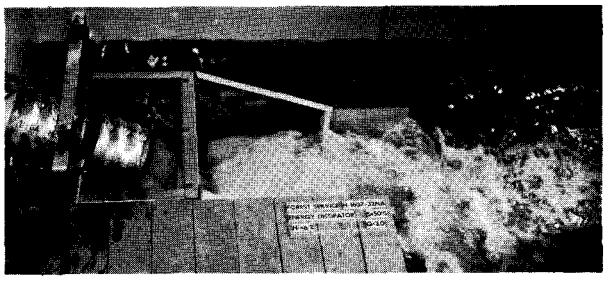
Figure 16. Helical corrugated-metal-pipe studies.



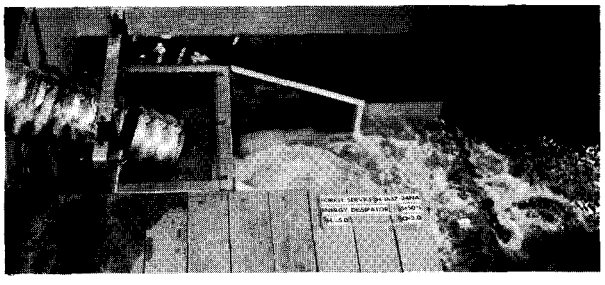
A. Q = 21.5 cfs, He = 8.0 feet, S = 50 percent. Note unacceptably rough flow. Photo PX-D-68537



B. Q = 17.4 cfs, He J7.2 feet, S = 50 percent. Note surges downstream from dissipator. Photo PX-D-68538



C. Q = 13.0 cfs, He = 6.2 feet, S = 50 percent. Acceptable flow. Photo PX-D-68539



D. Q = 8.7 cfs, He = 5.0 feet, S = 50 percent. Relatively smooth flow. Photo PX-D-68540

Figure 17. Acceptable and unacceptable flow. Note wave action on backwall of box.

Example to dimension an energy dissipator for an 18-inch corrugated-metal-pipe underdrain on a 30 percent pipe slope and a maximum discharge of 5.0 cfs: From Figure 18, the dimension factor is 0.56. Modify all linear dimensions shown in Figure 7, Basic Energy Dissipator, and the X_B–Y_B values in Figure 10 by the factor 0.56.

As a check on the application of the dimension factor chart, a 1:1.8 scale model of the energy dissipator for the above example was constructed and installed in the laboratory test box (Figures 19 and 20A). This comparatively small energy dissipator was tested for several pipe slopes and a range of discharges up to 5 cfs (Figure 20B). Energy dissipation was excellent for all pipe slopes and discharges tested.

Figures 7 and 18 are applicable without reservation for energy dissipators to be used with 18-inch corrugated-metal pipe underdrains.

Pipes other than 18 inches

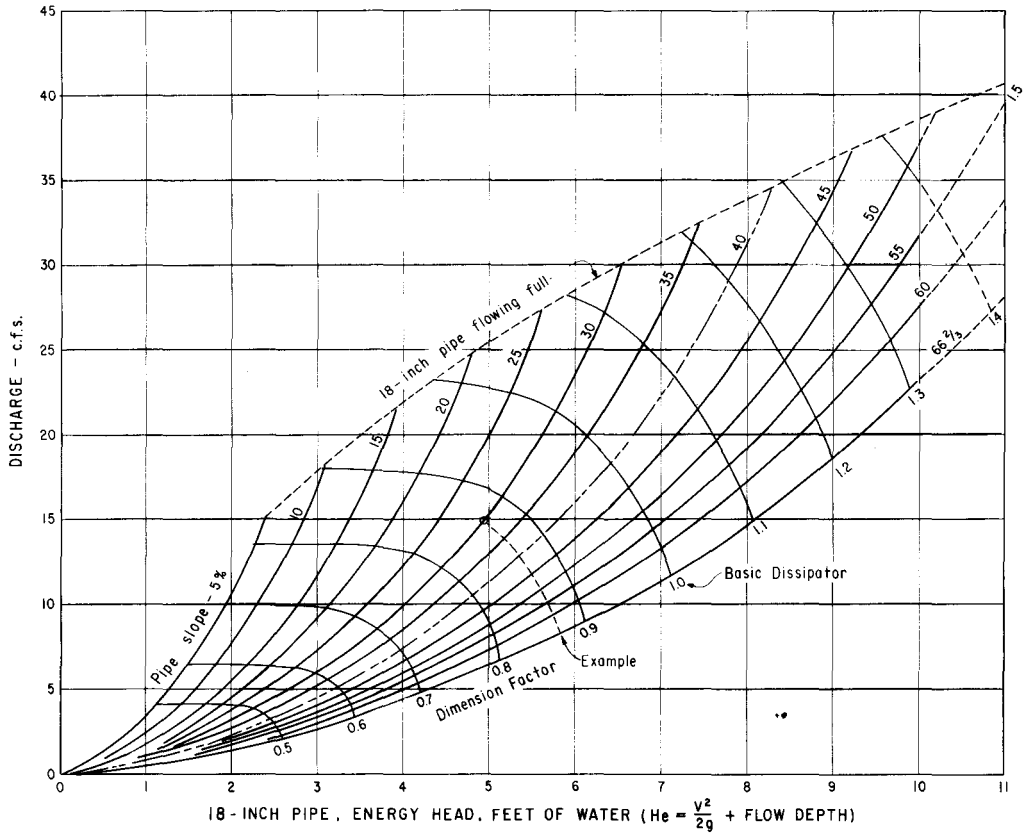
All dimensions and values in this report may be recomputed to generate parameters for corrugated-metal-pipe underdrains of sizes other than 18 inches. Values of the parameters for an 18-inch corrugated-metal pipe in Figures 7, 10, and 18 may be multiplied by a ratio "N" to determine companion parameters for the desired pipe size.

$$N = \frac{P}{18}$$

P = nominal corrugated-metal-pipe size (inches)

Parameter	Multiplier
Linear measurements	N
Energy head ($\frac{V^2}{2g}$ + depth)	N
Discharge	$N^{5/2}$
Pipe slope	1

The new charts generated from the computations could be applied to any desired corrugated-metal-pipe size. The author feels that the energy dissipator developed here should not be used for corrugated-metal-pipe sizes larger than 36 inches without further model studies.


DISCHARGE - c.f.s.
18-INCH PIPE, ENERGY HEAD, FEET OF WATER (He = V²/2g + FLOW DEPTH)
18-inch pipe flowing full
Pipe slope - 5%
Dimension Factor
Basic Dissipator
Example
0 5 10 15 20 25 30 35 40 45
0 1 2 3 4 5 6 7 8 9 10 11
0.5 0.6 0.7 0.8 0.9 1.0 1.1 1.2 1.3 1.4 1.5
10 15 20 25 30 35 40 45 50 55 60 66⅔

NOTES

For pipe slopes greater than 40%, deflector fillers must be used to achieve proper flow distribution and dissipator self cleaning capabilities.

For 40% pipe slope the dissipator operates equally well with or without fillers.

Dimension factor line is the upper limit of satisfactory operation for the discharge and pipe slope shown.

Example: For an 18-inch corrugated pipe installed on a 30% slope and discharging 15 cfs. the dimension of the basic energy dissipator, Figure 7, should be modified by the factor 0.87.

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Figure 18. Dimension Factor Chart for 18-inch corrugated pipe.

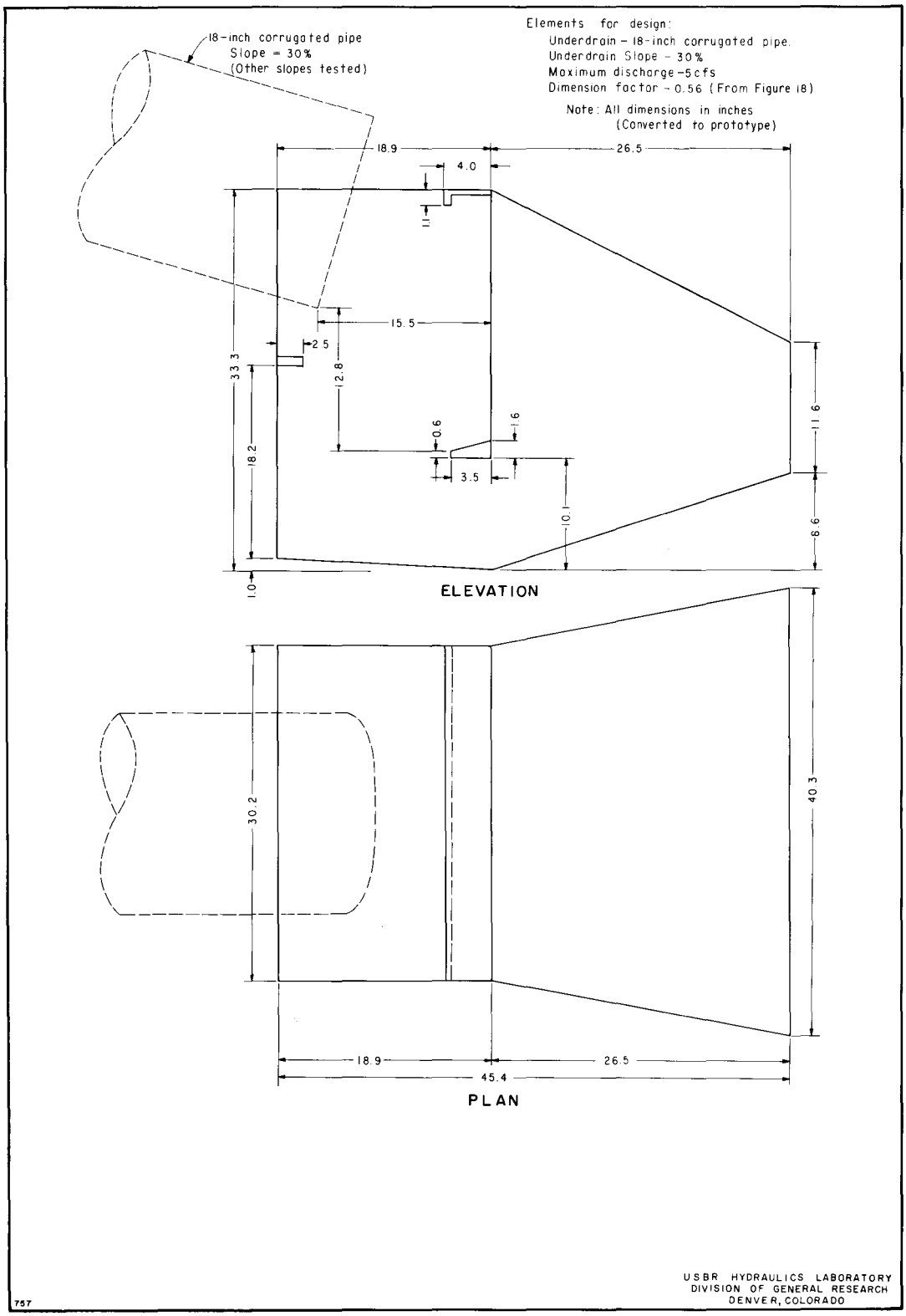

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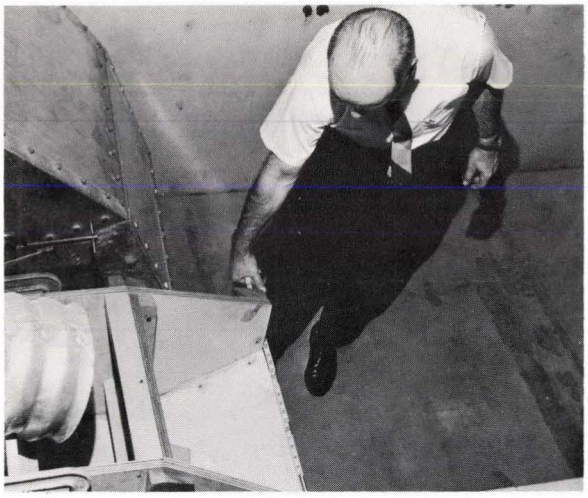
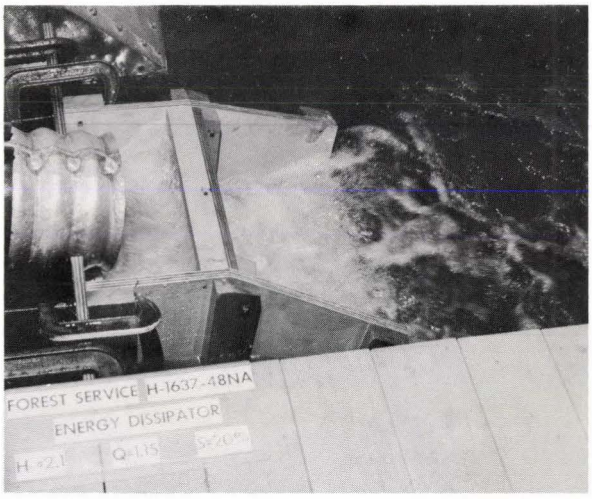
Figure 19. Energy dissipator for a dimension factor of 0.56.



A. Energy dissipator in the watertight box. Photo PX-D-68545



B. Q = 5.0 cfs; He = 2.1 feet; S = 20 percent. Photo PX-D-68546

Figure 20. Tests with an energy dissipator reduced by a factor of 0.56.

7-1750 (1-70)
Bureau of Reclamation

CONVERSION FACTORS--BRITISH TO METRIC UNITS OF MEASUREMENT

The following conversion factors adopted by the Bureau of Reclamation are those published by the American Society for Testing and Materials (ASTM Metric Practice Guide, E 380-68) except that additional factors (*) commonly used in the Bureau have been added. Further discussion of definitions of quantities and units is given in the ASTM Metric Practice Guide.

The metric units and conversion factors adopted by the ASTM are based on the "International System of Units" (designated SI for Systeme International d'Unites), fixed by the International Committee for Weights and Measures; this system is also known as the Giorgi or MKSA (meter-kilogram (mass)-second-ampere) system. This system has been adopted by the International Organization for Standardization in ISO Recommendation R-31.

The metric technical unit of force is the kilogram-force; this is the force which, when applied to a body having a mass of 1 kg, gives it an acceleration of 9.80665 m/sec/sec, the standard acceleration of free fall toward the earth's center for sea level at 45 deg latitude. The metric unit of force in SI units is the newton (N), which is defined as that force which, when applied to a body having a mass of 1 kg, gives it an acceleration of 1 m/sec/sec. These units must be distinguished from the (inconstant) local weight of a body having a mass of 1 kg; that is, the weight of a body is that force with which a body is attracted to the earth and is equal to the mass of a body multiplied by the acceleration due to gravity. However, because it is general practice to use "pound" rather than the technically correct term "pound-force," the term "kilogram" (or derived mass unit) has been used in this guide instead of "kilogram-force" in expressing the conversion factors for forces. The newton unit of force will find increasing use, and is essential in SI units.

Where approximate or nominal English units are used to express a value or range of values, the converted metric units in parentheses are also approximate or nominal. Where precise English units are used, the converted metric units are expressed as equally significant values.

Table I

QUANTITIES AND UNITS OF SPACE

Multiply	By	To obtain
LENGTH		
Mil	25.4 (exactly)	Micron
Inches	25.4 (exactly)	Millimeters
	2.54 (exactly)*	Centimeters
Feet	30.48 (exactly)	Centimeters
	0.3048 (exactly)*	Meters
	0.0003048 (exactly)*	Kilometers
Yards	0.9144 (exactly)	Meters
Miles (statute)	1,609.344 (exactly)*	Meters
	1.609344 (exactly)	Kilometers
AREA		
Square inches	6.4516 (exactly)	Square centimeters
Square feet	929.03*	Square centimeters
	0.092903	Square meters
Square yards	0.836127	Square meters
Acres	0.40469*	Hectares
	4,046.9*	Square meters
	0.0040469*	Square kilometers
Square miles	2.58999	Square kilometers
VOLUME		
Cubic inches	16.3871	Cubic centimeters
Cubic feet	0.0283168	Cubic meters
Cubic yards	0.764555	Cubic meters
CAPACITY		
Fluid ounces (U.S.)	29.5737	Cubic centimeters
	29.5729	Milliliters
Liquid pints (U.S.)	0.473179	Cubic decimeters
	0.473166	Liters
Quarts (U.S.)	946.358*	Cubic centimeters
	0.946331*	Liters
Gallons (U.S.)	3,785.43*	Cubic centimeters
	3.78543	Cubic decimeters
	3.78533	Liters
	0.00378543*	Cubic meters
Gallons (U.K.)	4.54609	Cubic decimeters
	4.54596	Liters
Cubic feet	28.3160	Liters
Cubic yards	764.55*	Liters
Acre-feet	1,233.5*	Cubic meters
	1,233,500*	Liters